

## HIGH PERFORMANCE INDUCER

### Cross Reference to Related Applications

**[0001]** This application claims priority from U.S. Provisional Patent Application Serial No. 60/527,334 filed December 05, 2003 and is incorporated herein by reference.

### Background of the Invention

**[0002]** This present invention relates to pumping assemblies, and finds particular application in pumping cryogenic materials, for example, where the pump assembly is immersed in fluid stored in a reservoir or container, such as a transport ship, and is required to pump the fluid from the bottom of the reservoir.

**[0003]** Pumps that embody inducers for liquid natural gas (LNG) applications such as LNG carrier loading pumps and primary send-out pumps are often required to operate at very low values of net positive suction head required (NPSHR) to facilitate the complete stripping of the storage tanks while maintaining full flow even while operating in full cavitation mode. Additionally, while operating at low tank levels, the pumps can ingest vapors caused by poor suction conditions and vortices. This results in two-phase flow regime.

**[0004]** Under such conditions, inducers in LNG pumps need to be capable of developing sufficient head (pressure) to compress these vapors sufficiently for reabsorption into the liquid in a hydrodynamically stable way. Otherwise, it is well known fact that the pump discharge pressure fluctuates when a column of vapor enters the pump inlet that is not fully reabsorbed. The presence of such fluctuations can cause vibration that can shorten pump life.

**[0005]** U.S. Patent No. Re 31,445, the details of which are incorporated herein by reference, is directed to a submersible pump assembly of the type for which the improved inducer or high performance inducer was developed. The '445 patent discloses a cryogenic storage system in which a reservoir, storage tank, tank car, tanker ship, etc., includes a casing suspended from an upper closure member or roof. Pipe sections extend from the roof and house a pump and motor unit that is positioned on a floor of the reservoir or storage container. Power is provided

through electrical cables and the entire pump and motor assembly is suspended via cable or rigid tubes or pipes.

**[0006]** A foot plate is provided on the lowermost end of the pump and motor assembly. Disposed inwardly from the bottom end is a flow inducer vaned impeller. As described in the '445 patent, a typical inducer impeller includes plural, circumferentially spaced vanes that extend radially outward from a central hub. This structure is generally referred to as a fan-type inducer. Still other manufacturers use a different impeller or inducer configuration such as a mixed flow inducer rather than the four blade fan-type inducer shown in the '445 patent.

**[0007]** Although known fan-type inducer and mixed flow inducer pumps have been used with some success in pump assemblies of this type, they encounter the above-described problem when used to pump a two-phase medium or fluid (i.e., liquid and vapor). As more air than liquid is drawn into the pump assembly because of the design, a substantial amount of the fluid is left in the reservoir. If LNG is shipped in a transport ship, for example, it is offloaded or pumped to a storage reservoir on shore. The inducer is an important element that needs to operate where very low inlet pressure is available. In LNG loading and primary send-out pumps, these conditions exist because the liquid in the tank is at or near saturation pressure (also referred to as true vapor pressure) when the level in the storage tank provides little submergence. In LNG secondary send-out pumps, these conditions can exist because the recondenser is at true vapor pressure when the pipe losses from the boil-off gas recondenser and the pump suction approach the elevation difference between the free liquid surface in the recondenser and the pump inlet (inducer eye).

**[0008]** When these conditions occur, the pressure in the inducer eye becomes equal to true vapor pressure, and any further pressure reduction will result in cavitation, producing bubbles or clouds of bubbles in the fluid. This occurs at the leading edge of the inducer blade when the relative velocity of the fluid with respect to the blade has any incidence angle other than zero. Under other conditions, vapor clouds can be ingested by the pump when suction vortice funnels open between the pump suction and the fluid free surface allowing a stream of vapor to flow into the pump suction. The ratio of vapor to liquid by volume is referred to as V/L or void fraction. The liquid/vapor mixture is two-phase flow. In extreme cases, clouds of bubbles or voids will block the flow and reduce pump output and efficiency.

**[0009]** Known inducer designs leave approximately four feet of LNG in the base of the reservoir of the transport ship. In other words, the reservoir of the ship is not sufficiently emptied and the transport ship is forced to carry residual LNG from the pumping station to a remote location where the transport ship is subsequently refilled. It is estimated that costs associated with this undesired retention and needless shipping of residual LNG that is not pumped from the transport container can cost approximately one hundred thousand dollars (\$100,000) per year per foot of residual LNG.

**[0010]** In light of the foregoing, it becomes evident that there is an appreciable need for an improved high performance inducer assembly that would provide a solution to one or more of the deficiencies from which the prior art has suffered. It is still more clear that an improved high performance inducer assembly providing a solution to each of the needs inadequately addressed by the prior art while providing a number of heretofore unrealized advantages thereover would represent a marked advance in the art. Accordingly, a need exists for an improved high performance inducer assembly and particularly an improved high performance inducer to significantly reduce the amount of residual LNG remaining in the ship reservoir after pump off. Likewise, a need exists for more efficient handling or pumping of a two-phase fluid.

#### **Brief Description of the Invention**

**[0011]** A new and improved high performance inducer for pumping cryogenic two phase fluids from reservoirs is provided.

**[0012]** More particularly, an inducer impeller for pumping cryogenic two phase fluids from reservoirs includes a hub with a first portion having a first diameter and a second portion with a second diameter larger than the first diameter. A plurality of primary and secondary blades is circumferentially disposed about the hub. Each secondary blade is interposed between two primary blades.

**[0013]** An inducer impeller of a downhole pump assembly for pumping a liquefied gas stored in a reservoir that includes two phase fluid components includes a plurality of primary blades extending from a hub. The primary blades have a generally helical conformation and are circumferentially spaced or disposed about the hub. Secondary blades extend from the hub and are interposed between the plurality of primary blades. The depth of the plurality of primary and secondary

blades is substantially greater at the first portion of the hub than at the second portion of the hub.

**[0014]** An inducer impeller for pumping a two phase fluid from a cryogenic storage system includes a hub which increases in diameter from a first portion to a second portion. Plural, axially extending primary blades each has a leading edge extending radially and axially from the hub. Axially extending secondary blades are circumferentially disposed about the hub such that one of the secondary blades is interposed between two adjacent primary blades. An outer diameter of each primary blade and each secondary blade is generally constant from a leading edge to a trailing edge of such primary and such secondary blades.

**[0015]** A primary benefit of the present invention resides in the ability to achieve a vapor-to-liquid ratio (V/L) of approximately 1:1.

**[0016]** Another benefit of the present invention resides in the ability to substantially reduce the retained or residual fuel left in a reservoir.

**[0017]** Still another benefit resides in the substantial savings associated with the ability to pump off a greater amount of LNG, i.e., to reduce the residual depth of remaining LNG in the reservoir.

**[0018]** Still other benefits and aspects of the invention will become apparent from a reading and understanding of the detailed description of the preferred embodiments hereinbelow.

#### **Brief Description of the Drawings**

**[0019]** The present invention may take physical form in certain parts and arrangements of parts, preferred embodiments of which will be described in detail in this specification and illustrated in the accompanying drawings which form a part of the invention.

**[0020]** FIGURE 1 is a longitudinal cross-sectional view of a prior pumping system disclosed in U.S. Re. 31,445 in which the high performance inducer of FIGURES 2-4 can be incorporated.

**[0021]** FIGURE 2 is a perspective view of the high performance inducer illustrating the hub and blade assembly according to the present invention.

**[0022]** FIGURE 3 is an elevational view of the inducer of FIGURE 2.

**[0023]** FIGURE 4 is a rear perspective view of the inducer hub and blade assembly of FIGURE 2.

**Detailed Description of the Invention**

**[0024]** It should, of course, be understood that the description and drawings herein are merely illustrative and that various modifications and changes can be made in the structures disclosed without departing from the spirit of the invention. Like numerals refer to like parts throughout the several views.

**[0025]** With reference to FIGURE 1 and as disclosed in U.S. Re. 31,445, a portion of a pump and motor unit **10** for a pumping system for pressurized cryogenic gas storage reservoirs in which an improved inducer of the present invention (to be described in greater detail below in connection with FIGURES 2-4) can be incorporated is illustrated.

**[0026]** As shown in FIGURE 1 and described in U.S. Re. 31,445, a conventional induction motor **12** has a vertical motor shaft **14** journalled at its upper end in an antifriction bearing (not shown) carried in an upwardly opening bushing (not shown). The motor shaft **14** is also typically journalled at its bottom end in an open topped cylindrical shell **16** in an antifriction bearing **18**. A first or bottom end of the shaft has a high performance inducer **20** mounted thereon and primary and secondary centrifugal vaned impellers **22** and **24** are keyed to the shaft **14** at axially spaced intervals above the flow inducer **20** to form the impellers of a two-stage pump **26**. The second stage impeller **24** is vented to the bearing **18** so that pumped fluid may flow from the top bearing (not shown) through the motor **12** to lubricate the lower bearing **18** and then drain through a vent **28** for reintroduction back to the fluid being pumped by the impeller **24**.

**[0027]** The high performance inducer **20** has a plurality of circumferentially spaced vanes **29** extending radially of a central hub **30** keyed to the lower end of the motor shaft **14** beneath a spacer **32** as by means of a key (not shown). The high performance inducer **20** thus spans the inlet of the pump and coacts with an inlet fitting **34** opening to the periphery of a foot plate **36** for a foot valve (not shown). This foot plate **36** has upstanding ribs (not shown) at spaced intervals, therearound carrying the shroud fitting **34** which abuts a rim **38** so that fluid flows over the plate **36** under the action of the inducer blades **29** to the primary and secondary impellers **22** and **24**.

**[0028]** The primary impeller **22** is of the double shrouded type and includes a central hub **40** abutting the top of the spacer **32** and is keyed to the shaft **14** for

corotation. The impeller has a first or top shroud **42** extending radially of the hub **40** to an inlet end of an annular passage **44** inside of a pump housing **46** and surrounding the impeller. A second or bottom shroud **48** coacts with the shroud **42** and with circumferentially spaced upstanding impeller vanes **50** to provide a pumping passage opening axially upward and then radially outward into the annular passageway **44**.

**[0029]** Vanes **52** extend radially across the annular passageway **44** at circumferentially spaced intervals and are effective to convert the velocity head from the impeller vanes **50** to a pressure head. The annular passageway **44** discharges beyond the vanes **52** into a flow passage **54** converging to the inlet end of the secondary impeller **24**. This secondary impeller is constructed and operates in the same manner as the primary impeller **22** and is driven by the shaft **14** in the same manner. The secondary impeller **24** discharges fluid upwardly through an annular passage **56** containing balancing vanes **58** similar to the vanes **52**. The fluid discharges out of an annular open top of the passage **56** into a casing **58** for upward flow therethrough to an outlet fitting (not shown).

**[0030]** Referring now to FIGURES 2-4, wherein the showings illustrate a preferred embodiment of the invention only and are not intended to limit same, FIGURE 2 illustrates an inducer **100**, which as noted above, can be incorporated in the pump and motor unit **10** for a pumping system for pressurized cryogenic gas storage reservoirs. The inducer of the present invention overcomes the problems associated with air so that once the pumped two phase medium has passed part way through the inducer the medium is a single phase liquid. This is achieved with the inducer design illustrated in FIGURES 2-4 and described herein.

**[0031]** More particularly, a central hub **110** of the inducer includes an opening **112** therethrough to secure the inducer to the drive shaft **14** extending from the motor **12**. The first end of the hub has a rounded end (i.e., no sharp edges or contours) and a curvilinear conformation that proceeds from the end as best seen in FIGURES 2 and 3, extending both generally radially outward from the shaft and extending axially therealong. The hub extends from a recess **114** formed in the end and curves outwardly to a first generally constant diameter hub portion **116**. Leading edges of first, second, and third helical blades **120a-120c** extend radially and axially outward from the hub - particularly extending from the constant diameter portion thereof. As will be appreciated, the leading edges **122a-122c** corresponding

to each of the blades is circumferentially spaced approximately  $120^\circ$  from the leading edge of the next adjacent blade. The thicknesses of the blades increases or tapers from the leading edges **122a-122c** to a substantially constant thickness over the remainder of the blades represented by reference numerals **124a-124c**, proceeding to respective trailing edges **126a-126c**. As is perhaps best represented in FIGURES 2 and 3, each blade is identical to the other blades and extends circumferentially approximately  $180^\circ$  from the leading edge **122a-122c** to the respective trailing edge **126a-126c**. Each blade has a helical or spiral conformation as it extends circumferentially about the hub and also extends axially from the generally constant diameter portion **116** of the hub toward an enlarged diameter portion of the hub **130** (FIGURES 3 and 4). As will be appreciated, the hub increases in diameter between the first or leading ends of the blades and the second or axially spaced trailing ends thereof. Stated another way, the hub contour is not simply a constant taper, and advantageously does not incorporate any sharp edges over its length.

**[0032]** Interposed between the three primary blades **120** are secondary or splitter blades. The splitter blades are situated to "carry" more flow through the inducer. Thus, by the time flow has reached the trailing end of the inducer, it is being pumped by six blades rather than the three original blades at the inlet end. The primary blades have a greater twist to aid in compressing the vapor and this increased twist also provides greater spacing in an axial direction (i.e., parallel or along the rotational axis) that accommodates the splitter blades. As noted, three splitter blades **150a, 150b, 150c** are provided, one between each of the primary blades. As perhaps best exemplified in FIGURES 2 and 4, leading edges **152** of the splitter blades are circumferentially spaced about  $60^\circ$  from the leading edge **122** of the primary blades. Each of the splitter blades also has a tapering leading edge **152** that merges into a more substantially constant thickness over the remaining circumferential extent of the blade profile. The circumferential extent from the leading edge **152** to the trailing edge **156** of each splitter blade is approximately  $150^\circ$ .

**[0033]** As is perhaps best illustrated in FIGURE 3, the hub continues to increase in diameter as it proceeds from the leading edge of the blade toward the trailing ends thereof. Where the flow exits each of the primary and splitter blades, however, the hub has a generally constant diameter and a smoothly rounded contour where it

terminates at the second end **160**. The configuration of the hub serves the purpose of a minimum back pressure at the leading edge. This makes it easy for the fluid to be introduced into the blades of the inducer. The high twist angle of the blades serves a compressor-like function, compressing the vapor so that the pumped medium is converted from a two-phase medium of both air and liquid to a single-phase or liquid by the time it exits the inducer. Thus, the blades, as well as the increasing diameter of the hub, provide this compressing action.

**[0034]** Whereas a fan-type inducer may achieve a vapor-to-liquid ratio (V/L) of 0.2 to 0.3 therethrough, and a mix flow inducer has a ratio of 0.4 to approximately 0.45, the inducer of the present invention has an approximately 1:1 ratio of the vapor-to-liquid (V/L).

**[0035]** The depth of the blade, i.e., the dimension of the blade measured in a generally radial direction from the hub out to the outer diameter edge of the blade is also quite different in accordance with the present invention. Whereas a mixed flow pump will typically have an increasing blade depth at the outlet than the depth at the leading edge, such is not the case in the present invention. Here, the depth of the blade measured from the hub to the tip is substantially greater at the inlet than at the outlet (see FIGURE 3). The outer diameter of the blade is essentially unchanged from the leading edge to the trailing edge, but since the hub diameter increases from the leading or inlet end to the trailing or outlet end, the depth of the blades decreases over this axial extent. As noted above, this configuration also contributes to the improved vapor-to-liquid pumping ratio of the inducer assembly.

**[0036]** Incorporating this inducer design into the pump assembly results in a substantial reduction in retained or residual fuel left in the reservoir. Whereas prior arrangements resulted in approximately four (4) feet (1.22 meters) of residual LNG remaining in the reservoir, the subject invention substantially reduces the residual depth to approximately eight (8) inches or 0.66 feet (0.2 meters). With an estimated cost of one hundred thousand dollars (\$100,000) per year per foot associated with transporting the LNG that has not been pumped from the ship reservoir, a substantial savings is associated with the ability to pump off a greater amount of LNG, i.e., to reduce the residual depth of remaining LNG in the reservoir.

**[0037]** This high vapor handling high performance inducer could be applied to handle boil-off gas problems in multi-stage high pressure pumps. Its excellent aero/hydrodynamic blade design makes it less susceptible to cavitation. Its high



pump head capability compresses any gas present, whether through entrainment or cavitation to be reabsorbed into the liquid phase. The high performance inducer will operate with stability at low flow rates at or even below 10% of rated flow, due to features of the design that control recirculation within the inducer. These capabilities offer the possibility that the high performance inducer could obviate the need for a recondenser with this inducer serving that purpose. The potential cost savings are potentially large.

**[0038]** The exemplary embodiment has been described with reference to the preferred embodiments. Obviously, modifications and alterations will occur to others upon reading and understanding the preceding detailed description. It is intended that the exemplary embodiment be construed as including all such modifications and alterations insofar as they come within the scope of the appended claims or the equivalents thereof.